On the Theory of Stable Mode of Dendritic Growth in the Presence of Convective Heat and Mass Transfer Boundary Conditions

DMITRI V. ALEXANDROV Ural Federal University Department of Theoretical and Mathematical Physics Laboratory of Multi-Scale Mathematical Modeling Lenin Avenue 51, 620000 Ekaterinburg RUSSIAN FEDERATION dmitri.alexandrov@urfu.ru

LIUBOV V. TOROPOVA Ural Federal University Department of Theoretical and Mathematical Physics Laboratory of Multi-Scale Mathematical Modeling Lenin Avenue 51, 620000 Ekaterinburg RUSSIAN FEDERATION

PETER K. GALENKO Friedrich-Schiller Universität Jena Physikalisch-Astronomische Fakultät Löbdergraben 32, D-07743 Jena GERMANY

Abstract: The dendritic form is one of the most common forms of crystals growing from supercooled melts and supersaturated solutions. In recent decades, an analytical theory has been developed that describes a stable dendrite growth mode under the conditions of a conductive heat and mass transfer process. However, in experiments, the growth of dendritic crystals is often observed under the conditions of convective fluid flow. In the present work, the theory of the growth of dendritic crystals is developed taking into account the convective mechanism of heat and mass transfer at the crystal-melt interface. A stable mode of dendritic growth in the case of intense convective flows near the steady-state growing dendritic tip is analyzed. The selection theory determining a stable growth mode in the vicinity of parabolic solutions as well as the undercooling balance condition are used to find the dendrite tip velocity and its tip diameter as functions of the melt undercooling. It is shown that the theoretical predictions in the case of convective and conductive heat and mass transfer mechanisms near the growing dendritic surfaces are compared. Our calculations show that the convective boundary conditions essentially influence the stable mode of dendritic growth.

Key-Words: Dendritic growth, Forced convection, Selection theory

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1 Introduction

Dendrites are one of the most common morphological formations that appear as a result of crystallization from the metastable liquid state of melts and solutions [1–8] (figure 1). The shape and kinetics of dendritic crystals depend on the anisotropy of the solid/liquid interface and the processes of heat and mass transfer [9–11]. The experimental data demonstrate that the internal structure of crystallized melts and solutions strongly depends on the metastability degree (undercooling or supersaturation), the crystallization rate, and the characteristic diameter of the dendrite vertices [12–14]. Convection in the liquid phase also plays an important role in the growth of dendritic crystals, changing the conditions of heat and mass transfer and leading to mechanical deformations of growth structures [15–17].

The authors of papers [18–20] show that convective fluid flows increase the crystallization rate, compress the thermal and concentration boundary layers, and also lead to an increase in the thermal and concentration gradients in front of growing dendritic crystals. These physical features are usually not taken into account in dendritic growth models. So, for example, a dendritic growth model is usually used with boundary conditions of the conductive type at the crystal/liquid interface [13, 21–28]. Such models describe a large number of experimental data for various Péclet and Reynolds numbers under the assumption of laminar flow in the liquid phase (or in the absence of flow).



Figure 1: A scheme of dendritic crystals.

However, there are experimental data on dendritic growth in liquids with intense (turbulent) flows at the interfacial boundaries of growing crystals [29, 30]. In this case, the mechanism of heat and mass transfer ceases to be conductive and is described by the boundary conditions of the convective type [29, 30].

This article discusses the influence of the boundary conditions of convective heat and mass transfer at the interfacial boundaries of dendritic crystals on the crystallization process. Namely, in this work, the theory of microscopic solvability is compared with experimental data on the growth of dendritic crystals from $Ti_{45}Al_{55}$ melts [19].

2 Stability Criterion for Convective Heat and Mass Transport

In this work, we will consider a low-speed crystallization process with intense fluid motion near the dendritic surface. In this case, the process of heat and mass transfer at the interface can be considered as convective, and the boundary conditions of the balance of heat and mass can be written in the form of convective-type conditions [29–31]. To find a selection criterion for a stable dendritic growth mode, we will use the boundary conditions in the presence of convective heat and mass transfer [31]. This type of heat and mass transfer mechanism occurs due to the turbulent flows near the solid/liquid interface [29, 30] or as a result of thermo-electrical hydrodynamic fluxes [12, 18] shown in figure 2.

The selection criterion determining a stable combination between the dendrite tip velocity V and its tip diameter ρ is given by [32]

$$\sigma^* \equiv \frac{2d_0 D_T}{\rho^2 V} = \frac{2\sigma_0 \sqrt{\alpha_d} D_T \beta_1}{\rho}$$



Figure 2: A scheme of dendritic growth in the presence of inrense convective flow. Arrows show the flow velocity.

$$+\frac{\sigma_0 \alpha_d^{5/4} (1+bD_T \beta_1) \left(1+\mu \tilde{\tau}_1^{3/2}\right)^2}{\left[1+\nu_1 \left(\rho b \alpha_d^{3/4}+\frac{3 \alpha_d^{1/4} P_g \beta_1 D_T}{2^{1/4} d_0}\right)\right]^2}.$$
 (1)

Here

$$\tilde{\tau}_1 = \frac{\alpha_d^{1/4} \rho b^2 d_0}{2^{1/4} P_g (1 + b D_T \beta_1)}, \ \beta_1 = \beta_0 + \frac{m C_i (1 - k_0)}{T_Q \alpha_s u_*},$$

$$b = \frac{\alpha_h \rho_l c_l u_*}{2k_s}, \ \nu_1^2 = \frac{2^{9/2} 25\sigma_0}{27},$$
$$C_i = \frac{\alpha_s u_* C_{l\infty}}{\alpha_s u_* - (1 - k_0)V}, \ P_g = \frac{\rho V}{2D_T},$$

where σ_0 is the solvability constant, d_0 is the capillary constant, ρ_l is the density of liquid, k_0 is the solute segregation coefficient, α_d is the surface energy stiffness, β_0 is the kinetic growth coefficient, μ is the selection parameter, m is the liquidus slope, c_l is the heat capacity, u_* is the friction velocity, T_Q is the hypercooling, and k_s is the thermal conductivity of solid. Here α_h and α_s are the convective heat and mass transfer coefficients, $\alpha_h/\alpha_s = (D_T/D_C)^n$ with 2/3 < n < 4/5 (D_T and D_C represent the thermal diffusivity and diffusion coefficient). WSEAS TRANSACTIONS on HEAT and MASS TRANSFER DOI: 10.37394/232012.2020.15.5

3 Undercooling Balance

The second condition connecting V and ρ is given by the undercooling balance that represents the sum of different contributions. So, the total undercooling ΔT takes the form [13]

$$\Delta T = \Delta T_T + \Delta T_C + \Delta T_R + \Delta T_K.$$
 (2)

The thermal contribution ΔT_T can be written out in the form

$$\Delta T_T = T_i - T_{l\infty} = \frac{T_Q V k_s}{\alpha_h \rho_l c_l u_* D_T},\tag{3}$$

where T_i and $T_{l\infty}$ represent the temperatures at the interface and far from it.

The contribution ΔT_C arising from the solute concentration field reads

$$\Delta T_C = m(C_i - C_{l\infty}) = \frac{(1 - k_0) V m C_{l\infty}}{\alpha_s u_* - (1 - k_0) V}, \quad (4)$$

where C_i and $C_{l\infty}$ stand for the solute concentrations at the interface and far from it.

The contributions ΔT_R and ΔT_K appearing due to the interface curvature (the Gibbs-Thomson effect) and the attachement kinetics of atoms at the interface take the form

$$\Delta T_R = \frac{4d_0 T_Q}{\rho}, \ \Delta T_K = \frac{V}{\mu_k},\tag{5}$$

where μ_k is the kinetic coefficient.

Combining expressions (2)-(5), we obtain the following explicit function

$$\rho(V) = \frac{4d_0 T_Q}{\Delta T - \Delta T_T(V) - \Delta T_C(V) - \frac{V}{\mu_k}}.$$
 (6)

Now combining the selection criterion (1) and the modified undercooling balance (6), we arrive at the following implicit function determining the dendrite tip velocity V

$$\frac{\rho^2(V)V}{2d_0 D_T} \sigma^* \left(\rho(V), V \right) = 1, \tag{7}$$

where σ^* is defined by the right-hand side of expression (1).

Thus, expression (7) determines the dendrite tip velocity V as a function of total undercooling ΔT . The dendrite tip diameter ρ as a function of ΔT can be found from the modified undercooling balance (6).



Figure 3: Dendrite tip velocity versus the melt undercooling for Ti₄₅Al₅₅ alloy. The dashed (blue) and dash-dotted (green) lines show the results for the conductive mechanism of heat and mass transfer in the absence (U = 0 m/s) and presence (U = 0.5 m/s) of forced convective flow [34]. The solid line (red) is plotted accordingly to the present model (expression (7)). Theoretical predictions are compared with experimental data [19] for small undercoolings. The model parameters used in calculations are $\sigma_0 = 1.17$, $d_0 = 9.28 \cdot 10^{-10}$ m, $D_T = 2.5 \cdot 10^{-6}$ m² s⁻¹, $\rho_l = 2.46 \cdot 10^3 \text{ kg m}^{-3}, k_0 = 0.86, C_{l\infty} = 55 \text{ at\%},$ $\alpha_d = 0.3, \, \beta_0 = 1.88 \cdot 10^{-2} \text{ sm}^{-1}, \, \mu = 10^{-3}, \, m = 10^{-3}$ 8.78 K at%⁻¹, $c_l = 1237$ J kg⁻¹ K⁻¹, $\alpha_h = 3.55$, $u_* = 4 \text{ m s}^{-1}, T_Q = 272.64 \text{ K}, k_s = 29.22 \text{ W m}^{-1}$ \mathbf{K}^{-1} .

In the case of conductive heat and mass transfer boundary conditions the selection criterion takes the form [7,32,33]

$$\sigma^* = \frac{\sigma_0 \alpha_d^{7/4}}{1 + \tilde{b} \left(\alpha \alpha_d^{-3/4} \right)^{11/14}}$$
(8)

$$\times \left\{ \frac{1}{\left[1 + a_1 \sqrt{\alpha_d} P_g \left(1 + \frac{\delta_0 D_T \beta_0}{d_0}\right)\right]^2} \right. \\ \left. + \frac{2mC_i (1 - k_0) D_T}{\left[1 + a_2 \sqrt{\alpha_d} P_C \left(1 + \frac{\delta_0 D_C \beta_0}{d_{0CD}}\right)\right]^2 T_Q D_C} \right\},$$



Figure 4: The dendrite tip diameter versus its tip velocity. Panel (a) compares the convective and conductive heat and mass transfer mechanisms. Panel (b) shows the ingluence of friction velocity on ρ and V. Parameters used in calculations are $\alpha_h = 0.0095$, $k_s = 2.03 \text{ W m}^{-1} \text{ C}^{-1}$, $\rho_l = 10^3 \text{ kg m}^{-3}$, $c_l = 4187$ W s kg⁻¹, $d_0 = 2.8 \cdot 10^{-10} \text{ m}$, $\alpha_d = 0.35$, $\sigma_0 = 0.17$, $D_T = 1.17 \cdot 10^{-7} \text{ m}^2 \text{ s}^{-1}$, $\mu = 0$, $\beta_1 = \beta_0 = 0$.

where

$$\begin{aligned} a_1 &= \left(\frac{8\sigma_0}{7}\right)^{1/2} \left(\frac{3}{56}\right)^{3/8}, \ P_0 = P_g + P_f, \\ P_C &= \frac{\rho V}{2D_C}, \ a_2 = \sqrt{2}a_1, \\ \alpha &= \frac{ad_0 U}{4\rho V P} + \frac{ad_0 U D_T}{2\rho V P D_C}, \ P &= 1 + \frac{2mC_i(1-k_0)D_T}{D_C T_Q}, \\ C_i &= \frac{C_{l\infty} D_C}{D_C - (1-k_0) \exp\left(\frac{P_0 D_T}{D_C}\right) P_g I_C(\infty) D_T}, \\ d_{0CD} &= \frac{T_Q d_0}{2mC_i(1-k_0)}, \\ a(\Re) &= \sqrt{\frac{\Re}{2\pi}} \frac{\exp\left(-\Re/2\right)}{\exp\left(-\Re/2\right)} \text{ in } 2D, \\ a(\Re) &= \frac{\exp\left(-\Re/2\right)}{E_1\left(\Re/2\right)} \text{ in } 3D, \\ \delta_0 &= 20\sqrt{\frac{7}{24}} \left(\frac{56}{3}\right)^{3/8}, \ E_1(q) = \int_q^{\infty} \frac{\exp(-u)}{u} du, \end{aligned}$$

U is the fluid velocity at infinity, $P_f = \rho U/(2D_T)$, \tilde{b} is the stability constant, $\Re = \rho U/\nu$ is the Reynolds number, ν is the kinematic viscosity, and $I_C(\infty)$ is determined in [32].

Criterion (8) should be supplemented with the corresponding undercooling balance condition, which coincides with expression (2) with contributions ΔT_T , ΔT_C , ΔT_R , and ΔT_K found in [32] for two- and three-dimensional geometries.

The convective and conductive heat and mass transfer conditions [34] are compared with experimental data [19] in figure 3. Note that the theoretical predictions obtained in [34] are in good agreement with experiments only in the range of moderate and large undercoolings (see, for details, [34]). If we are dealing with the case of small growth velocities, the theory based on conductive-type boundary conditions does not agree with experimental data (the theoretical curves shown in figure 3 by the dashed and dashdotted lines lie outside of the experimental error bars). However, the convective heat and mass transfer mechanism at the solid/liquid boundary leads to the function $V(\Delta T)$ (solid line in figure 2) that corresponds to the experimental error bars at small undercoolings. Indeed, in the case of intense fluid flows around the growing dendrites, one can expect a transition from the laminar regime to the turbulent regime in levitated droplets [35]. This transition can be explained by the fact that the intense fluid curls lead to the convective heat and mass transfer mechanism in the vicinity of dendritic tips where the flow is strongly turbulent [35].

In figure 4, we illustrate the influence of convective boundary conditions on dendritic growth. The convective curve (dotted line) lies above the corresponding conductive curve (solid line). In other words, the dendrite tip diameter is greater in the case of convective heat and mass transfer than in the case of the conductive transfer mechanism. The greater values of friction velocity u_* also lead to larger values of the dendrite tip diameter.

4 Conclusion

In summary, the theory of stable dendritic growth in a binary melt with allowance for the convective heat and mass transfer mechanism at the solid/liquid surfaces of dendritic tips was developed. The theoretical predictions are compared with experiments and previous theory based on the conductive heat and mass transfer boundary conditions. The convective type of heat and mass transfer around the growing solid surfaces arises in a thin boundary layer, where the liquid moves chaotically so that the conductive heat and mass fluxes should be changed by Newtonian boundary conditions. Their main features consist of the fact that the heat and mass fluxes at the growing solid surfaces become convective and depend on the friction velocity u_* .

To test the theory with convective boundary conditions, we used two equations for the theoretical determination of the dendrite tip velocity and its tip diameter: the selection criterion and the undercooling balance. These equations are reduced to a single one defining an implicit function $V(\Delta T)$. This function was tested against experimental data in the range of small undercoolings. The velocity-undercooling dependence based on the convective heat- and mass transfer mechanism well describes experiments on the solidification of Ti₄₅Al₅₅ for small undercoolings.

As a final note, the mechanism of heat and mass transfer near the growing dendritic surfaces can be of a mixed type, i.e. it can contain the convective and conductive fluxes. Such a theory containing the mixed type of heat and mass transfer at the dendritic boundary can be developed on the basis of the present analysis and previous theory summarized in [36–39]. This subject represents a new research direction for future investigations.

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